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# How knowledge discovery and embedded paradigm transform industrial process management: exploring pipeline hydraulic dynamic identification

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## Abstract

An effective hydraulic parameter identification underpins process simulation for pipeline optimization. However, current studies often overlook the hydraulic spatiotemporal dynamics and multi-frequency variations of simulation parameters, limiting accuracy and interpretability. Here, by exploring the opportunity of bridging industrial process simulation relying on theoretical research paradigms in scientific discovery, we propose a knowledge discovery and embedded framework to identify optimal friction coefficient and capture multi-frequency online variations of friction. The proposed framework identifies the optimal friction coefficient by discovering hydraulic spatiotemporal dynamics based on partial derivative differences within pipeline hydraulic state matrices. By embedding explicit hydraulic physical theory into forward propagation, a physics-constrained autoregressive neural network is developed as an efficient, interpretable surrogate model. Then, a self-coordination framework is designed for synchronous friction updating. The proposed framework can achieve precise online hydraulic simulation by performing knowledge-discovery identification and knowledge-embedded modeling. Results confirm accuracy and robustness of the proposed framework across varying pipeline and fluid properties. By integrating bottom-up knowledge discovery with top-down embedding, this approach forms a self-improving loop, offering strong potential for industrial pipeline digital twins and efficient decision-making.

## 1 Introduction

Pipeline transportation systems, fundamental to various industrial sectors, have emerged as the most economical and energy-efficient solution for liquid media distribution, including urban water supply [1, 2] and petroleum product delivery [3, 4]. However, with infrastructure aging and replacement often delayed, frequent switching of operation conditions [5] can induce extreme pressure surges. These transient processes heighten the risk of structural failure and potential explosions [6], particularly in hydrocarbon pipelines due to their flammable and explosive nature [7]. Therefore, effective monitoring of pressure and flowrate is critical to maintaining system safety and reliability.

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High-precision sensors are commonly employed to monitor hydraulic states such as pressure and flowrate within pipelines. However, their widespread deployment is limited by substantial installation and maintenance costs, restricting sensor placement to locations such as pipeline inlets and outlets [8]. This sparse arrangement creates extensive non-detection zones within the pipeline system [9]. As a result, the development of efficient simulation tools capable of accurately estimating transient hydraulic states (pressure and flowrate) becomes essential for pipeline risk assessment [10, 11], system planning [12], and operational optimization [13, 14].

Hydraulic transients are governed by one-dimensional water hammer PDEs [15], which lack analytical solutions [16], prompting decades of research into numerical methods such as the Method of Characteristics (MOC) [17] and Finite Difference Method (FDM) [18]. In practice, wave propagation characteristic is influenced by uncertainties in PDE coefficients, including friction, wave speed, and pipe-wall viscoelasticity, which significantly impact simulation accuracy [19]. While most coefficients remain relatively constant and can be estimated empirically, the friction coefficient exhibits strong time dependence and is tightly coupled with transient dynamics. Accurate identification of friction coefficient play a pivotal role in reliable hydraulic simulation.

The optimization theory-based method, a prevalent framework for pipeline parameter identification, which identifies unknown parameters by aligning observed signals with associated numerical model outputs, was first introduced by Liggett and Chen in 1994 [20]. Optimization theory-based method primarily fall into two categories: mathematical statistical-based [21, 22] and evolutionary optimization-based [23, 24, 25], with the latter increasingly recognized as a leading technique due to its adaptability and robustness. However, conventional evolutionary strategies typically identify simulation parameters based solely on squared errors (SE) between measured and simulated responses. The essence that variations in parameters are often manifestations of deeper spatiotemporal hydraulic dynamics (*nonlinear time-delay characteristics and wave-propagation characteristics*) are neglected by conventional evolutionary strategies. This disconnect limits both the physical interpretability and the precision of hydraulic simulation under transient conditions. Additionally, the inherently iterative nature of evolutionary algorithms requires repeated PDE evaluation and population regeneration. This results in significant computational overhead, resulting in the incapability of parameter dynamics synchronous extraction [26].

Recently, time-series data-driven methods [27], such as the Nonlinear AutoRegressive neural network with eXogenous inputs (NARX) [25] and long short-term memory (LSTM) [28], have attracted significant interest in pipeline hydraulic simulation. These models can predict hydraulic parameters at pipeline inlets and outlets efficiently but struggle to infer states in non-detection zones. Moreover, the absence of hydraulic principles in their training leads to reduced accuracy and limited physical interpretability [29]. Physics-informed neural networks (PINNs) offer a promising solution by incorporating physical laws for more accurate and interpretable simulations [4]. However, their training is computationally intensive, which often requires several hours, thus limiting their practicality for real-time applications [30]. Meanwhile, although efficient hydraulic simulation can be achieved by data-driven methods, the high time cost of evolutionary iterations in parameter identification have not been fundamentally overcome.

The essence of identifying parameter is discovering the spatiotemporal hydraulic dynamics from pipeline system states. Motivated by the intrinsic spatiotemporal dynamics of hydraulic transient, this study explores the opportunity of bridging industrial process simulation relying on theoretical research paradigms in scientific discovery. We propose a novel knowledge discovery and embedded framework for interpretable parameter identification and precise hydraulic simulation. The key contributions of this work are as follows:

- To the best of our knowledge, we present the first spatiotemporal dynamic discovery-based parameter identification (STDD) algorithm (Sec 2.2.1) by designing a spatiotemporal partial derivatives to represent pipeline hydraulic dynamics. The proposed algorithm can identify friction coefficient effectively and overcome key limitations of existing techniques, including limited interpretability and degraded fidelity under transient conditions.
- We propose a physics-guided autoregressive neural network (PG-ARNN, Sec 2.2.2) that incorporates hydraulic transient theory to function as an efficient surrogate for parameter identification. Surrogate models can avoid the high iterative search costs of traditional parameter identification methods. This hybrid approach addresses the generalization limitations of purely data-driven models when exposed to previously unseen operating conditions.

- We develop a multi-frequency self-coordination simulation framework (Sec 2.2.3) by organically integrating knowledge discovery-driven identification with knowledge-informed modeling. This approach can capture multi-frequency synchronous variations in the friction coefficient. Then, the intrinsic asynchrony arising from fixed-interval parameter identification under both pseudo-steady and transient conditions can be better addressed.

## 2 Methodology

### 2.1 Problem description

As shown in Eqs. (1) and (2), the one-dimensional governing equations describe the transient hydraulic behavior in liquid pipelines as functions of both time ( $t$ ) and space ( $x$ ):

$$\frac{1}{gA} \left( \frac{\partial Q}{\partial t} + \frac{Q}{A} \frac{\partial Q}{\partial x} \right) + \frac{\partial H}{\partial x} + fQ|Q|^{1-m} = 0 \quad (1)$$

$$\frac{\partial H}{\partial t} + \frac{Q}{A} \frac{\partial H}{\partial x} + \frac{a^2}{gA} \frac{\partial Q}{\partial x} = 0 \quad (2)$$

where  $H$  is the head (pressure is the product of density, gravitational acceleration, and head),  $Q$  is the flowrate.  $A$  is the cross-sectional area of the pipeline,  $g$  is gravitational acceleration,  $f$  is the Darcy–Weisbach friction factor. The coefficient  $m$  is assigned as 0.25 for the hydraulically smooth zone and 0.125 for the mixed friction zone.  $a = \sqrt{\frac{K/\rho}{1 + \frac{K}{E} \frac{D}{8} C_1}}$  is the wave speed. For the other letters in the formula, see Reference [4].

Given the superior stability of pressure transmitters over ultrasonic flow meters, measured pressures are employed as inputs and boundary control conditions to drive the hydraulic simulation through MOC (Appendix A.1). The hydraulic simulation can be mathematically represented as  $X_{t+1} = F(X_t, U_{t+1})$ . Where  $X_t = [H_{0,t}, H_{1,t}, \dots, H_{M,t}, Q_{0,t}, Q_{1,t}, \dots, Q_{M,t}]$  denotes the system state matrix at  $t$ ,  $U_{t+1} = [H_{0,t+1}, H_{M,t+1}]$  is the boundary control conditions at  $t+1$ ,  $F(x)$  is the state update function. In practical applications,  $\Delta t$  is typically set to 1 second for real-time simulation, while  $\Delta x$  is derived from the wave speed and  $\Delta t$ .

As discussed in *Discussion of conventional parameter identification methods* in Appendix A.1, to tackle the identification asynchronism in real-time simulation and inherent overlook of spatiotemporal hydraulic dynamics of conventional methods, this study proposes an interpretable objective function and a multi-frequency self-coordination simulation framework.

### 2.2 Data-driven knowledge discovery and embedded framework

#### 2.2.1 Spatiotemporal Dynamic Discovery-Based Parameter Identification Algorithm

The friction coefficient is closely linked to the Reynolds number, which depends on fluid properties and flowrate [18]. Under transient conditions, rapid fluctuations in pressure and flowrate cause corresponding changes in friction. Accurately identifying the optimal friction coefficient in real time is therefore crucial for precise hydraulic simulation.

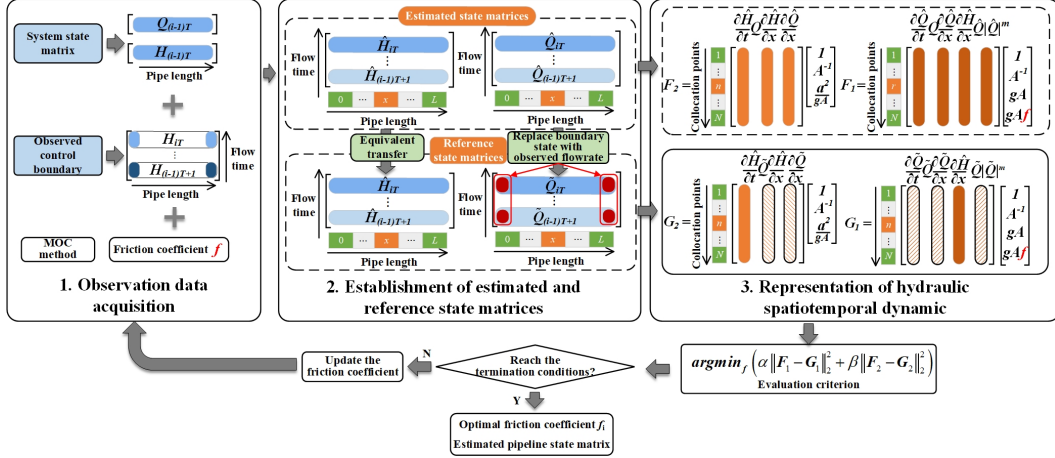


Figure 1: Spatiotemporal Dynamic Discovery-Based Parameter Identification Framework

As depicted in Figure 1, to identify the friction coefficient, the initial condition is treated as pseudo-steady, with hydraulic states  $H(x, t)$  and  $Q(x, t)$ ,  $x \in [0, L]$ ,  $t \in [-m, 0]$ , where  $L$  is the pipeline length and  $m$  denotes the duration of pseudo-steady flow along the pipeline derived using Darcy's law. Let  $T$  represent the parameter identification interval. Given boundary conditions  $H(x, t)$  in the  $i^{th}$  interval, with  $x \in \{0, L\}$  and  $t \in [(i-1)T+1, iT]$  as well as initial states  $H(x, t)$  and  $Q(x, t)$  with  $x \in [0, L]$  and  $t = (i-1)T$ , the state matrices can be estimated via the hydraulic simulation described in Sec 2.1, as shown in Eqs. (3) and (4).

$$\hat{H} = \begin{bmatrix} H(0, iT) & H(1, T) & \cdots & H(L, T) \\ H(0, iT-1) & H(1, iT-1) & \cdots & H(L, iT-1) \\ \vdots & \vdots & \ddots & \vdots \\ H(0, (i-1)T+1) & H(1, (i-1)T+1) & \cdots & H(L, (i-1)T+1) \end{bmatrix} \quad (3)$$

$$\hat{Q} = \begin{bmatrix} Q(0, iT) & Q(1, T) & \cdots & Q(L, T) \\ Q(0, iT-1) & Q(1, iT-1) & \cdots & Q(L, iT-1) \\ \vdots & \vdots & \ddots & \vdots \\ Q(0, (i-1)T+1) & Q(1, (i-1)T+1) & \cdots & Q(L, (i-1)T+1) \end{bmatrix} \quad (4)$$

Observed flowrates are acquired from calibrated ultrasonic flow meters. Substituting the boundary flowrates in the estimated flowrate matrices (Eq. (4)) with observed values yields the reference flowrate matrix, as shown in Eq. (5).

$$\tilde{Q} = \begin{bmatrix} \tilde{Q}(0, iT) & Q(1, T) & \cdots & \tilde{Q}(L, T) \\ \tilde{Q}(0, iT-1) & Q(1, iT-1) & \cdots & \tilde{Q}(L, iT-1) \\ \vdots & \vdots & \ddots & \vdots \\ \tilde{Q}(0, (i-1)T+1) & Q(1, (i-1)T+1) & \cdots & \tilde{Q}(L, (i-1)T+1) \end{bmatrix} \quad (5)$$

Notably, the reference head matrix is the same as the estimated head matrix. When the friction coefficient used in hydraulic simulation aligns well with actual hydraulic dynamics, the estimated and reference flowrate matrices should closely coincide. To evaluate hydraulic dynamic differences, the partial derivatives of elements in both estimated ( $\hat{H}$  and  $\hat{Q}$ ) and reference ( $\tilde{H}$  and  $\tilde{Q}$ ) matrices over time and space are discretized using finite difference schemes, yielding the residuals of the water hammer PDEs, as shown in Eqs. (6)–(9).

$$F_1 = \Phi_1^{est} \bullet \xi_1^{est} = \left[ \nabla_t \hat{Q}, \hat{Q} \bullet \nabla_x \hat{Q}, \nabla_x \hat{H}, \hat{Q} \mid \hat{Q} \right]^{0.75} \left[ 1, \frac{1}{A}, gA, gAf \right]^T \quad (6)$$



$$F_2 = \Phi_2^{est} \bullet \xi_2^{est} = \left[ \nabla_t \hat{H}, \hat{Q} \nabla_x \hat{H}, \nabla_x \hat{Q} \right] \left[ 1, \frac{1}{A}, \frac{a^2}{gA} \right]^T \quad (7)$$

$$G_1 = \Phi_1^{ref} \bullet \xi_1^{ref} = \left[ \nabla_t \tilde{Q}, \tilde{Q} \bullet \nabla_x \tilde{Q}, \nabla_x \hat{H}, \tilde{Q} |\tilde{Q}|^{0.75} \right] \bullet \left[ 1, \frac{1}{A}, gA, gAf \right]^T \quad (8)$$

$$G_2 = \Phi_2^{ref} \bullet \xi_2^{ref} = \left[ \nabla_t \hat{H}, \tilde{Q} \nabla_x \hat{H}, \nabla_x \tilde{Q} \right] \left[ 1, \frac{1}{A}, \frac{a^2}{gA} \right]^T \quad (9)$$

Here,  $\nabla$  denotes the gradient operator for head and flowrate, while  $\Phi^{est}$  and  $\Phi^{ref}$  form libraries of partial derivative and constant terms for the estimated and reference matrices, respectively.  $F_1 \in \mathbb{R}^{N \times 4}$  and  $F_2 \in \mathbb{R}^{N \times 3}$ , with  $N = L \times T$  being the number of collocation points, represent the momentum and continuity residuals for the estimated matrices; likewise,  $G_1 \in \mathbb{R}^{N \times 4}$  and  $G_2 \in \mathbb{R}^{N \times 3}$  are the corresponding residuals for the reference matrices. When the friction coefficient reflects the true hydraulic behavior, the spatiotemporal derivatives of both matrices coincide, resulting in equal residuals. Accordingly, an objective function (Eq. (10)) is proposed to quantify the residual differences.

$$\{f^*, H^*(x, t), Q^*(x, t)\} = \underset{f}{\operatorname{argmin}} \left( \alpha \|F_1 - G_1\|_2^2 + \beta \|F_2 - G_2\|_2^2 \right) \quad (10)$$

Here,  $\alpha$  and  $\beta$  are tunable hyper-parameters used to enhance convergence effect. Solving the optimization yields the optimal friction coefficient  $f^*$ , along with the corresponding hydraulic states  $H^*(x, t)$  and  $Q^*(x, t)$  in non-detectable pipeline zones. Finally, the STDD algorithm is executed periodically to update the friction coefficient in different time intervals, ensuring the hydraulic simulation remains aligned with pipeline dynamics. In essence, STDD advances parameter identification method by quantifying hydraulic spatiotemporal dynamics (**time-delay and wave-propagation characteristics**), thereby enhancing physical interpretability. By replacing the objective function (Eqs. (3)-(10)) in Figure 1 as squared error (SE, Eq. (17)), conventional parameter identification methods can be acquired.

### 2.2.2 Physics-Guided Autoregressive Neural Network

While Sec 2.2.1 introduces a interpretable parameter identification algorithm, the real-time applicability of STDD is hindered by its high computational cost (on the order of minutes). To address this, we propose a computationally efficient surrogate model that replicates STDD's functionality. Based on the Reynolds Transport Theorem, liquid properties and present flowrate are primary determinants of the friction coefficient. However, as present flowrates are not boundary control conditions, they must be inferred from previous hydraulic states and present pressure data. To this end, a dual-layer neural network framework is constructed (Figure A.1), employing autoregressive neural networks in each layer to capture time-delay characteristics in hydraulic parameters. The first-level network takes the estimated boundary flowrate from  $(i-1)T$  to  $iT$  and the observed boundary pressure from  $(i-1)T$  to  $(i+1)T$  as inputs to predict flowrate in the interval  $iT$  to  $(i+1)T$ .

Then, the estimated present flowrate of the first-level network is concatenated with previous flowrate as input features. This composite input, along with the friction coefficient at the  $i^{th}$  interval, are fed into the second-level network. Additionally, fluid density and viscosity are processed via a fully connected (FC) layer to infer the friction coefficient at the  $(i+1)^{th}$  interval. The forward propagation of the dual-lay neural network is detailed in Appendix A.2.

### 2.2.3 Multi-Frequency Self-Coordination Simulation Framework

The temporal variability of the friction coefficient, a key determinant of hydraulic simulation accuracy, differs markedly between pseudo-steady and transient conditions. In pseudo-steady states, friction changes minimally over minutes to hours, whereas transient conditions induce second-scale fluctuations. Optimization-based parameter identification approaches, including STDD, which require minutes for parameter identification, suffer from significant phase lag during transients. To address

this, we propose an multi-frequency self-coordination simulation framework, detailed in Framework 1.

Initially, optimal friction coefficients and estimated states obtained via STDD at two different time intervals are used to train separate PG-ARNNs. Among these, STDD with time interval being 10 seconds for transient and 5 minutes for pseudo-steady conditions. Operation conditions are identified by comparing pressure fluctuation amplitudes against predefined thresholds, triggering the corresponding PG-ARNN. When the cumulative sampling time surpasses the designated interval, observed pressure and estimated states are used to identify the friction coefficient. Otherwise, the previous friction is retained. This updated coefficient is then applied for real-time hydraulic simulation, enabling an online rolling simulation.

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**Framework 1** Online hydraulic simulation by using a multi-frequency self-coordination framework

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**Offline Training:**

**1. For time intervals of 10-second or 5-minutes:**

- 1.1 Extract the observed boundary pressure and previous hydraulic states along pipeline
- 1.2 Identify the optimal friction and simulate the hydraulic states
- 1.3 Form friction databases (**D<sub>1</sub> for 10-second interval, D<sub>2</sub> for 5-minute interval**)
2. Train different PG-ARNNs using databases (**D<sub>1</sub>→PG-ARNN<sub>1</sub>, D<sub>2</sub>→PG-ARNN<sub>2</sub>**)

**Online Simulation:**

1. Gather real-time pressure and previous estimated hydraulic states
  2. If the pressure fluctuation exceeds predefined threshold
    - 2.1 Recognized as transient condition and a **10-second interval** is applied
    - 2.2 If cumulative sampling time surpasses the designated interval
      - 2.2.1 Identify friction coefficient using **PG-ARNN<sub>1</sub>**
      - 2.3 Else, **using the historical friction coefficient**
      - 2.4 Hydraulic simulation
  3. Else
    - 3.1 Recognized as pseudo-steady condition and a **5-minute interval** is applied
    - 3.2 If cumulative sampling time surpasses the designated interval
      - 3.2.1 Identify friction coefficient using **PG-ARNN<sub>2</sub>**
      - 3.3 Else, **using the historical friction coefficient**
      - 3.4 Hydraulic simulation
  4. Begin hydraulic simulation in next time step
- 

### 3 Case studies with experiments

#### 3.1 Experiment setting

To evaluate the effectiveness and generalizability of the proposed framework, four real-world liquid pipelines with varying characteristics were selected, as detailed in Table B.1. All pipelines share a common elasticity modulus of  $2.07 \times 10^{11}$  Pa. As illustrated in Figure B.1, pressure signals recorded at the pipeline inlet and outlet by high-precision sensors were used as input to the hydraulic simulation model, enabling estimation of pressure and flowrate at  $\Delta x$  km intervals at 1-second resolution. Flowrate data from calibrated ultrasonic flowmeters at both ends were employed for STDD execution and validation of flowrate simulations. Pressure measurements from three intermediate valve chambers between pipeline inlet and outlet supported pressure simulation verification.

The optimal network parameters of PG-ARNN were determined via trial and error, as shown in Table B.2. The model was implemented using the PyTorch framework. To optimize the balance between performance and computational efficiency of STDD, 50 iterations were performed with 50 candidate coefficients evaluated per iteration. PG-ARNN was trained over 2000 epochs with an initial learning rate of 0.0001. The experiments were conducted on a workstation equipped with a single NVIDIA GeForce RTX 3090 GPU.

#### 3.2 Evaluation and analysis of the proposed STDD algorithm

Optimization-based parameter identification methods primarily differ in their iterative strategies and evolutionary mechanisms, as their underlying objective functions are essentially the same. In

this study, we mainly focus on proposing a novel objective function for evolution iteration process. Consequently, this subsection only analyzes identification results derived from different objective functions. The SE-based method, which replaces the objective function in STDD as SE are selected as benchmark. To demonstrate the significance of parameter identification, the hydraulic simulation model based on MOC without parameter identification is used as comparative model.

The hydraulic simulations on Case 1 are illustrated in Figure 2. and 3. STDD delivers the most accurate hydraulic simulation, closely aligning with observed profiles and outperforming all comparative methods. In contrast, the MOC approach exhibits the largest discrepancies. While SE-based and STDD methods show similar accuracy during pseudo-steady states, STDD demonstrates markedly superior performance under transient conditions. Flowrate and pressure simulation on other three cases are shown in Figure B.2 and B.4. Figure B.3, B.5, Table 1, and 2 further support this, with STDD achieving the lowest pressure residuals, with average errors being 0.0013 MPa, 0.0011 MPa, 0.0034 MPa, and 0.0042 MPa across four cases. By exploiting hydraulic dynamics characteristics of spatiotemporal derivatives, STDD reduces residuals by 81.9%, 60.7%, 87.5%, and 40.0% compared to SE-based method.

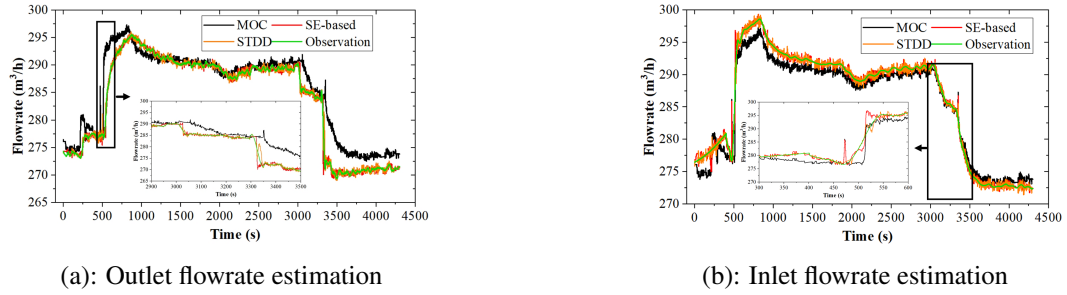


Figure 2: Comparison of flowrate estimation between SE-based method and STDD on Case 1

Table 1: MAPE comparisons of flowrate estimation between SE-based method and STDD

Methods	Inlet flowrate estimation (%)			Outlet flowrate estimation (%)		
	Whole flow process	Transient condition	Pseudo-steady condition	Whole flow process	Transient condition	Pseudo-steady condition
STDD	<b>0.085</b>	<b>0.299</b>	<b>0.082</b>	<b>0.079</b>	<b>0.193</b>	<b>0.070</b>
MOC	0.415	1.084	0.344	0.700	2.417	0.603
SE-based	0.108	0.795	0.098	0.121	0.463	0.109

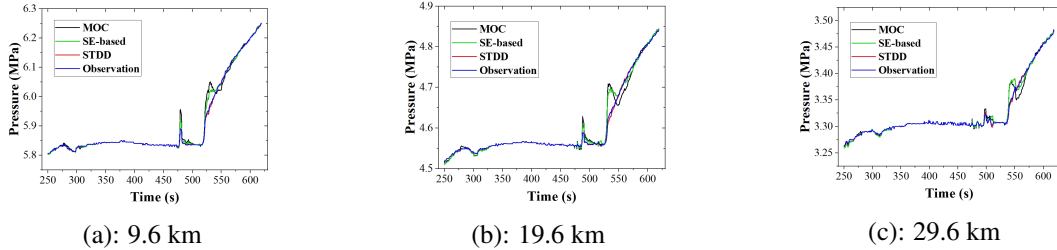


Figure 3: Comparison of flowrate estimation between SE-based method and STDD on Case 1

Table 2: Average absolute residuals of pressure simulation between SE-methods and STDD

Cases	Average absolute residuals (MPa)		
	MOC	SE-based	STDD
Case 1	0.0135	0.0072	<b>0.0013</b>
Case 2	0.0043	0.0028	<b>0.0011</b>
Case 3	0.0338	0.0272	<b>0.0034</b>
Case 4	0.0090	0.0070	<b>0.0042</b>

Table 3: Flowrate estimation errors of different frameworks

Flowrate estimation	Frameworks	Inlet flowrate estimation (%)			Outlet flowrate estimation (%)		
		Whole flow process	Transient condition	Pseudo-steady condition	Whole flow process	Transient condition	Pseudo-steady condition
Outlet flowrate	Proposed Framework (PG-ARNN)	<b>0.283</b>	<b>1.204</b>	<b>0.296</b>	<b>0.097</b>	<b>0.291</b>	<b>0.169</b>
	Proposed Framework (NARX)	0.402	1.683	0.530	0.391	0.875	0.624
	Conventional Framework	0.609	3.803	0.708	0.639	1.017	0.727
Inlet flowrate	Proposed Framework (PG-ARNN)	<b>0.395</b>	<b>0.693</b>	<b>0.422</b>	<b>0.112</b>	<b>0.351</b>	<b>0.151</b>
	Proposed Framework (NARX)	0.443	0.837	0.533	0.176	0.465	0.195
	Conventional Framework	0.565	1.447	0.589	0.455	1.956	0.620

Table 4: Average absolute residuals of pressure simulation between various frameworks

Cases	Average absolute residuals (MPa)		
	Conventional Framework	Proposed Framework (NARX)	Proposed Framework (PG-ARNN)
Case 3	0.0277	0.0114	<b>0.0025</b>
Case 4	0.0194	0.0124	<b>0.0024</b>

To provide a comprehensive interpretability analysis of the spatiotemporal dynamics identification algorithm, the identification results and the trend of hydraulic parameters over time are discussed in the appendix C.1.

### 3.3 Evaluation of PG-ARNN and multi-frequency simulation framework

To demonstrate the importance of multi-frequency parameter identification for online simulation, we compare the proposed frameworks (with either PG-ARNN or the benchmark NARX model) to a conventional fixed-interval (5 min) parameter identification approach. Neural networks are trained on Cases 1–2 and tested on Cases 3–4, ensuring a balanced dataset split.

As shown in Figure B.6 and B.8, the simulation results of conventional framework on Case 3 exhibits the largest deviations from observed values. These errors stem from phase delays in fixed-interval parameter identification, which fail to capture rapid friction coefficient fluctuations during transients. In contrast, the proposed multi-frequency approach enables high-frequency updates during transients, enhancing estimation accuracy. Residual error comparisons in Figure B.7 and B.9 further support this. Quantitative results in Table 3 and 4 confirm that PG-ARNN achieves the lowest errors, reducing inlet flowrate MAPE by 68.4% and 71.4% compared to the conventional framework. For the pressure simulation, PG-ARNN-based framework suggests a residual reduction of 91.0% and 87.7% compared to the conventional framework, and 78.0% and 80.7% compared to NARX-based framework.

## 4 Discussion and Conclusion

In this study, we propose a innovative data-driven knowledge discovery and embedded framework for interpretable parameter identification and accurate pipeline hydraulic simulation. The primary advantages and innovations are summarized as follows:

- Our approach constructs partial derivative residuals across spatial and temporal domains of system state matrices for discovering hydraulic spatiotemporal dynamics. These form the basis of the parameter identification algorithm with an interpretable objective function. The proposed algorithm tackles the limitations that estimate hydraulic states inaccurately, especially under transient conditions. Real-world cases show that pipeline transients exhibit substantial hydraulic spatiotemporal dynamic variability. Across four benchmark cases,

our algorithm reduces MAPE in transient inlet and outlet flowrate by 53.1% and 63.5%, respectively, and improves pressure prediction by 81.9%, 60.7%, 87.5%, and 40.0%.

- We develop a physics-constrained neural network by embedding discovered hydraulic laws into forward propagation, serving as an efficient surrogate for parameter identification. Building on this, a multi-frequency online simulation framework is introduced to enable synchronous parameter updates. Dynamic adjustment of identification intervals effectively eliminates the phase delay issues inherent in fixed-interval-based methods. Compared to conventional frameworks, the proposed method reduces MAPE by 68.35% (inlet) and 52.15% (outlet) in Case 3, further improving to 71.37% and 82.08% in Case 4. For pressure prediction, residuals drop by 91.0% and 87.7%, respectively.

This approach offers a novel pathway for digital twin development in process simulation of pipeline operation by uncovering hidden physics and reintegrating it to enhance model fidelity. Future efforts will aim to develop efficient multi-dimensional hydrodynamic interaction tensors and advance high-accuracy, low-cost simulation algorithms.

## 5 Acknowledgment

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## A Supplementary Material of Proposed Method

### A.1 Hydraulic simulation of liquid pipeline based on MOC

**Hydraulic simulation process** Using the MOC method, the transient hydraulic characteristic equations are derived through simplification and linear combination, as presented in Eqs. (11) and (12).

$$C^+ : \begin{cases} \frac{dx}{dt} = a \\ \frac{a}{gA} \frac{dQ}{dt} + \frac{dH}{dt} + fQ|Q|^{1-m} a = 0 \end{cases} \quad (11)$$

$$C^- : \begin{cases} \frac{dx}{dt} = -a \\ \frac{a}{gA} \frac{dQ}{dt} - \frac{dH}{dt} + fQ|Q|^{1-m} a = 0 \end{cases} \quad (12)$$

Due to the non-differentiability of the friction terms in the characteristic equations, finite difference schemes are employed to approximate the spatial derivatives in Eqs. (11) and (12), as shown in Eqs. (13) and (14). The pipeline is discretized into segments ( $\Delta x = L/M$ ), and the flow is computed over time steps ( $\Delta t = \Delta x/a$ ).

$$C^+ : \frac{a}{gA} (Q_{i,t+1} - Q_{i-1,t}) + (H_{i,t+1} - H_{i-1,t}) + fQ_{i,t+1}|Q_{i-1,t}|^{1-m} a \Delta t = 0 \quad (13)$$

$$C^- : \frac{a}{gA} (Q_{i,t+1} - Q_{i+1,t}) - (H_{i,t+1} - H_{i+1,t}) + fQ_{i,t+1}|Q_{i+1,t}|^{1-m} a \Delta t = 0 \quad (14)$$

Simultaneously solving Eqs. 13 and 14 establishes the relationship between variables at time  $t+1$  and  $t$ , as expressed in Eqs. 15 and 16.

$$Q_{i,t+1} = \frac{R^+ - R^-}{S^+ + S^-} \quad (15)$$

$$H_{i,t+1} = R^+ - S^+ Q_{i,t+1} \quad (16)$$

where  $R^+ = H_{i-1,t} + C_W Q_{i-1,t}$ ,  $R^- = H_{i+1,t} - C_W Q_{i+1,t}$ ,  $S^+ = C_W + f|Q_{i-1,t}|^{1-m} a \Delta t$ ,  $S^- = C_W + f|Q_{i+1,t}|^{1-m} a \Delta t$ ,  $C_W = \frac{a}{gA}$ . Thus, by specifying any two of the flowrate and pressure values at the pipeline inlet and outlet boundaries at time  $t+1$ , the hydraulic state along the pipeline at that moment can be determined.

**Discussion of conventional parameter identification methods** To estimate the friction coefficient and optimal states, existing parameter identification methods address the inverse problem by minimizing the squared error (SE) between estimated and observed flowrates over a time interval  $T$ :

$$\hat{f} = \underset{f}{\operatorname{argmin}} \left( \sum_{t=1}^T (Q_{0,t}^{est} - Q_{0,t}^{obs})^2 + \sum_{t=1}^T (Q_{M,t}^{est} - Q_{M,t}^{obs})^2 \right) \quad (17)$$

Conventional objective function (Eq. (17)) overlook the central role of the friction factor in governing spatiotemporal hydraulic dynamics. Existing parameter identification methods typically identify parameters using data from a fixed interval (e.g., 20 minutes) and apply them to the subsequent interval, leading to estimation deviations, especially in real-time transients where hydraulic conditions evolve within seconds. This study thus proposes an interpretable evaluation criterion (Eq. (17)) to enable synchronous parameter identification for real-time simulation.

## A.2 Forward and backward propagation in PG-ARNN

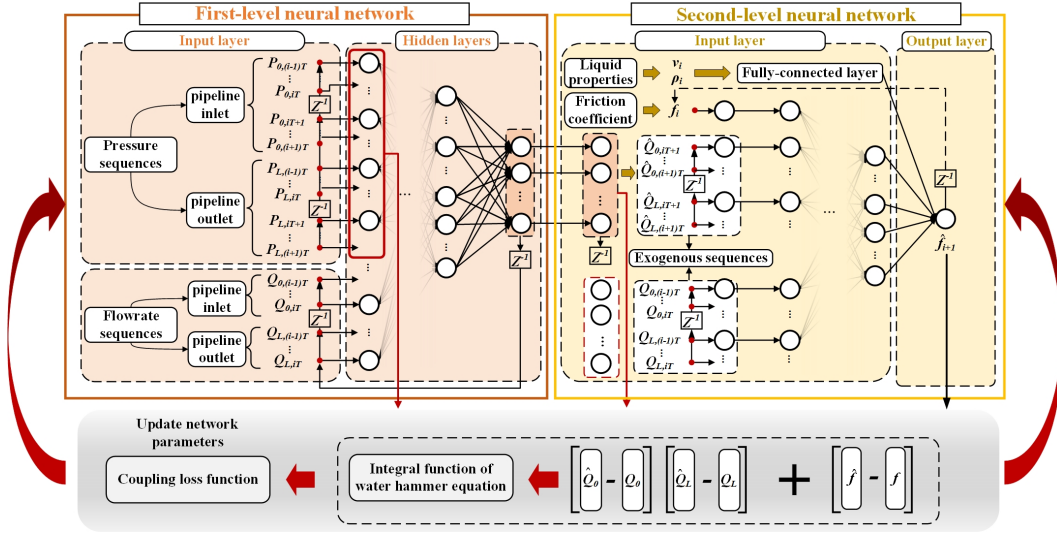


Figure A.1: Schematic diagram of PG-ARNN

As depicted in Figure A.1, the first-level network takes the estimated boundary flowrate from  $(i-1)T$  to  $iT$  and the observed boundary pressure from  $(i-1)T$  to  $(i+1)T$  as inputs to predict flowrate in the interval  $iT$  to  $(i+1)T$ , as defined in Eq. (18).

$$(Q_{0,iT+1}, \dots, Q_{0,(i+1)T}, Q_{L,iT+1}, \dots, Q_{L,(i+1)T}) = MAN_1 \left( \begin{array}{c} Q_{0,(i-1)T}, \dots, Q_{0,iT}, Q_{L,(i-1)T}, \dots, Q_{L,iT}, \\ P_{0,(i-1)T}, \dots, P_{0,(i+1)T}, P_{L,(i-1)T}, \dots, P_{L,(i+1)T}; \theta_1 \end{array} \right) \quad (18)$$

where  $MAN_1$  is the multilayer autoregressive neural network in the first layer, and  $\theta_1$  is the trainable parameters in the neural network of the first layer.  $Q_{0,t}$  and  $Q_{L,t}$  represent the flowrate in the pipeline inlet and outlet.  $P_{0,t}$  and  $P_{L,t}$  represent the pressure in the pipeline inlet and outlet.

The estimated present flowrate of the first-level network is concatenated with previous flowrate as input features. This composite input, along with the friction coefficient at the  $i^{th}$  interval, is fed into the second-level network. Additionally, fluid density and viscosity are processed via a fully connected (FC) layer to infer the friction coefficient at the  $(i+1)^{th}$  interval. The forward propagation of this second-level network is detailed from Eqs. (19)–(21).

$$Z_1 = MAN_2 \left( Q_{0,(i-1)T}, \dots, Q_{0,(i+1)T}, Q_{L,(i-1)T}, \dots, Q_{L,(i+1)T}, f_i; \theta_2 \right) \quad (19)$$

$$Z_2 = W_{fc}X + b_{fc} \quad (20)$$

$$\hat{f}_{i+1} = W_o(Z_1 \oplus Z_2) + b_o \quad (21)$$

where  $X$  represents the input matrix consisting of liquid properties elements.  $\theta_2$  is the trainable parameters in the neural network of the second layer.  $(W_{fc}, b_{fc})$  and  $(W_o, b_o)$  are the weights and biases in the FC layer and output layer.  $\oplus$  represents the feature-wise concatenation. where  $\hat{f}_{i+1}$  is the observed friction coefficient.

The mean squared errors (MSE) between predicted and observed results of first and second-level networks can be represented as:



$$L_{first} = \frac{1}{N} (\|FLN_{Q_L} - Q_L\|_2^2 + \|FLN_{Q_0} - Q_0\|_2^2) \quad (22)$$

$$L_{seond} = \frac{1}{N} \|SLN_f - f\|_2^2 \quad (23)$$

To end with, the coupling loss function  $L = L_{seond} + L_{first}$  can be used to train the dual-layer neural network.

## B Supplementary Figures and Tables

Table B.1: The properties of example pipelines and transported liquids

Cases	Pipeline properties			Liquid properties		
	Outer diameter (mm)	Length (km)	Wall thickness (mm)	Density ( $\text{kg}\cdot\text{m}^{-3}$ )	Viscosity ( $\text{mmPa}\cdot\text{s}$ )	Volume elasticity modulus(Pa)
Case 1	406.4	39.9	7.1	742	0.72	$9.2\times 10^8$
Case 2	323.9	55.1	6.4	753	1.12	$4.2\times 10^8$
Case 3	219.1	32.1	5.6	825	5.33	$1.5\times 10^9$
Case 4	219.1	45.7	5.6	821	5.27	$1.3\times 10^9$

Table B.2: The hyper-parameter setting of PG-ARNN

Network section	Hyper-parameters	Range	Time interval	
			10 seconds	5 minutes
First-level network	Number of layers	1-10	3	5
	Neural units	10-3000	[100, 50]	[2000, 500, 10]
	Batch size	16-512	256	512
	Activation function	[Relu, Tanh, Sigmoid]	Relu	Relu
	Dropout	0-0.5	0.1	0.1
Second-level network	Number of layers	1-10	2	2
	Neural units	8-128	[60, 20]	[700, 100]
	Batch size	10-1000	256	512
	Activation function	[Relu, Tanh, Sigmoid]	Relu	Relu
	Dropout	0-0.5	0.1	0.1

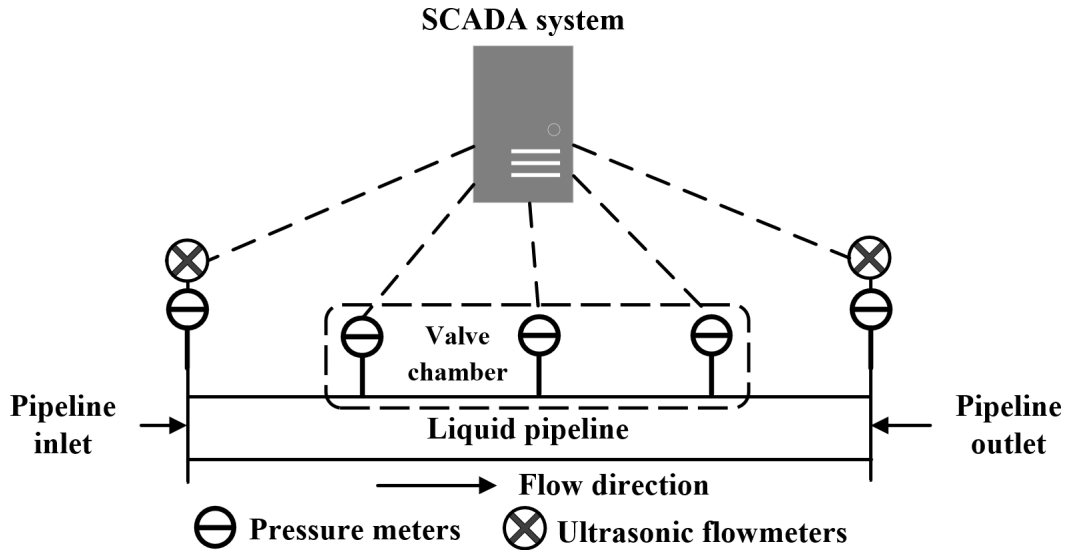
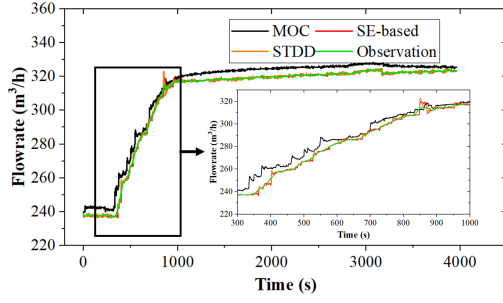
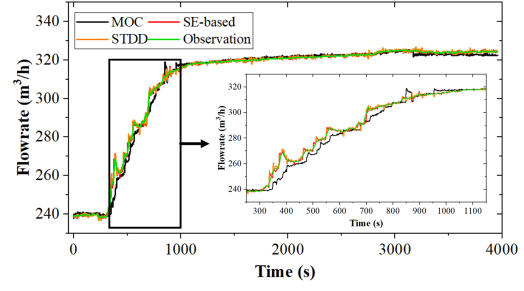


Figure B.1: Schematic diagram of liquid pipeline (SCADA: Supervisory Control and Data Acquisition system)

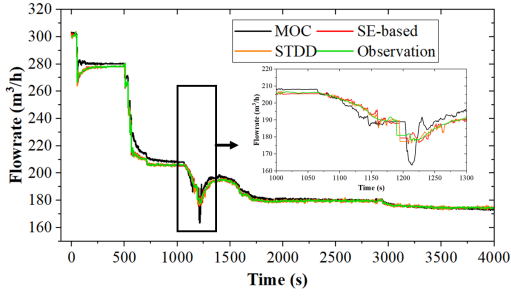


(i) Inlet flowrate estimation

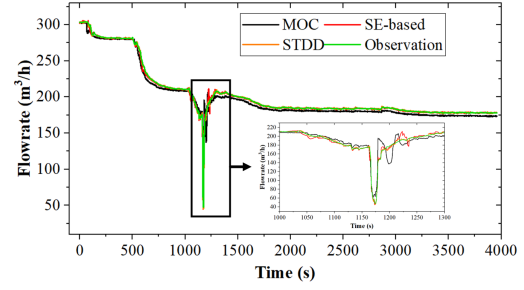


(ii) Outlet flowrate estimation

(a) Case2

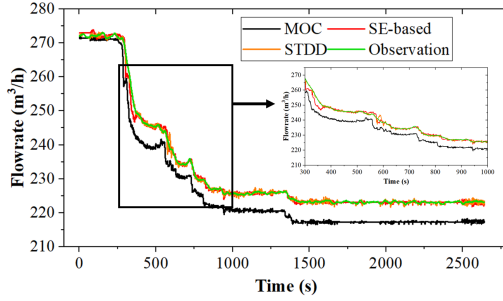


(i) Inlet flowrate estimation

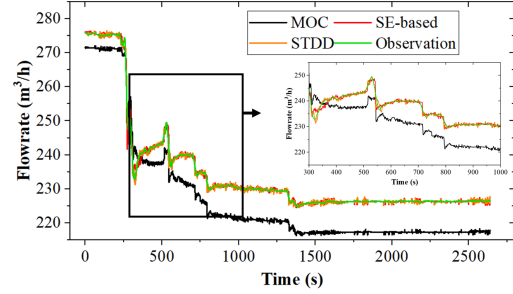


(ii) Outlet flowrate estimation

(b) Case 3



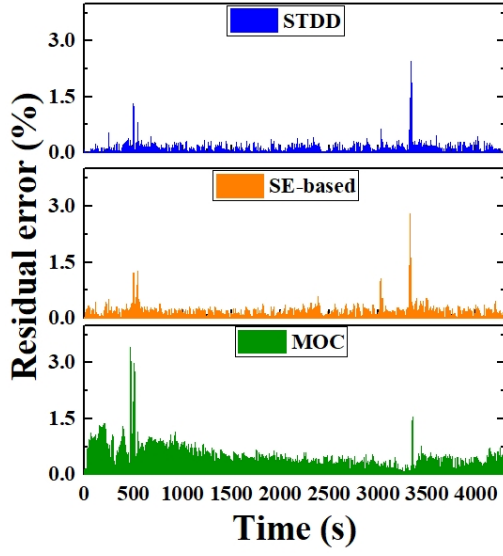
(i) Inlet flowrate estimation



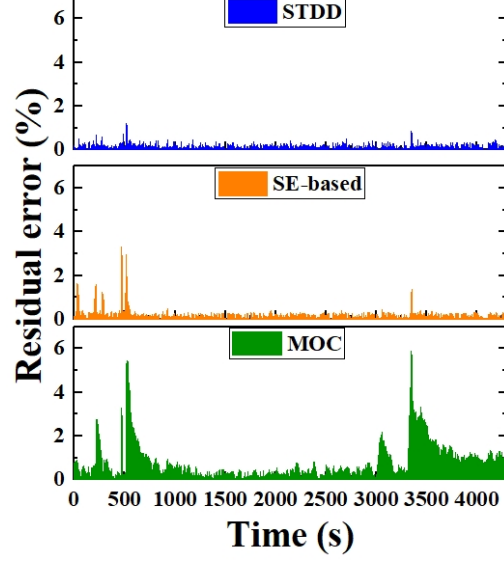
(ii) Outlet flowrate estimation

(c) Case4

Figure B.2: Visualization comparison of flowrate estimation between SE-based method and STDD

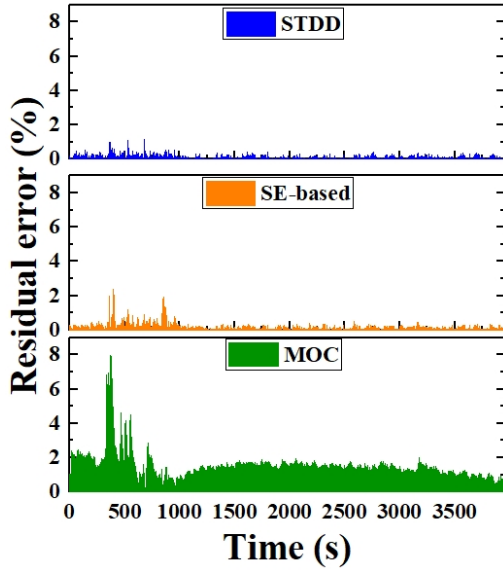


(i) Inlet flowrate estimation

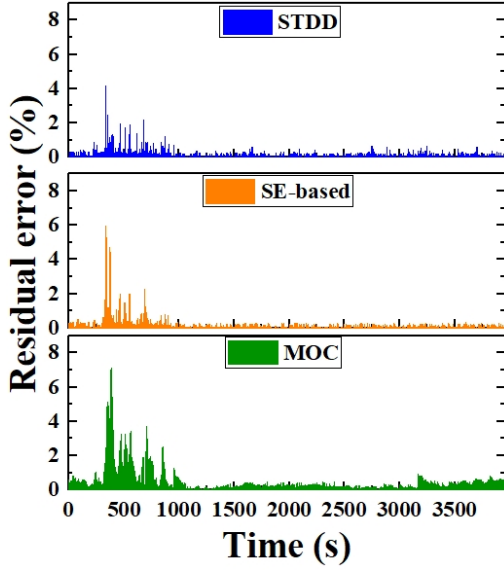


(ii) Outlet flowrate estimation

(a) Case1

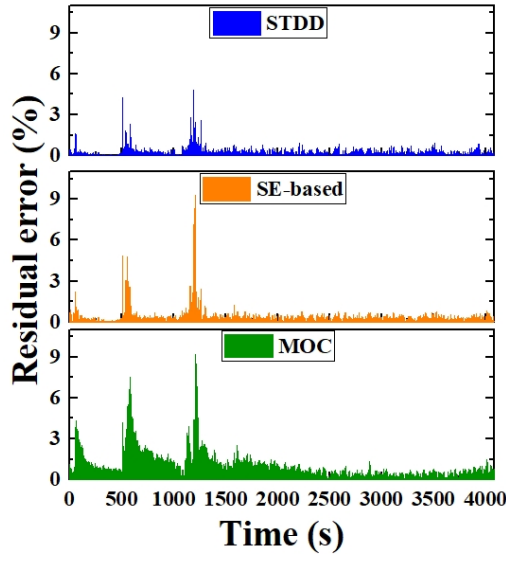


(i) Inlet flowrate estimation

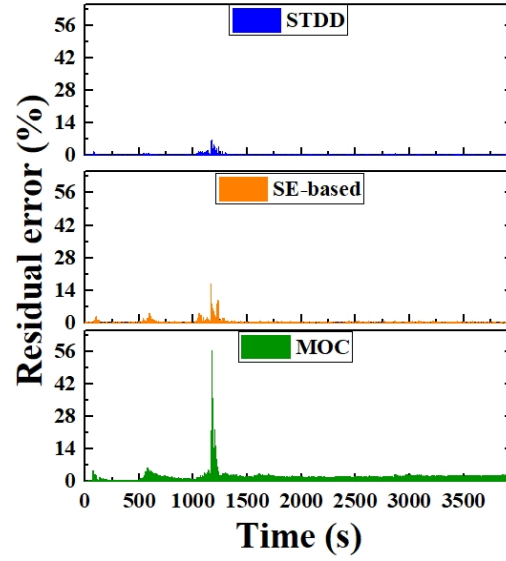


(ii) Outlet flowrate estimation

(b) Case2

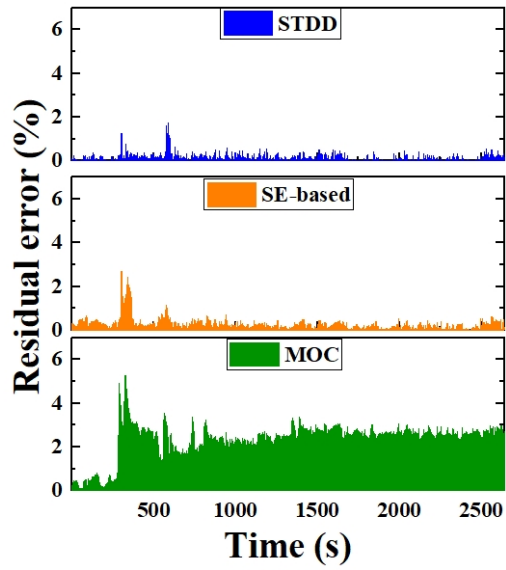


(i) Inlet flowrate estimation

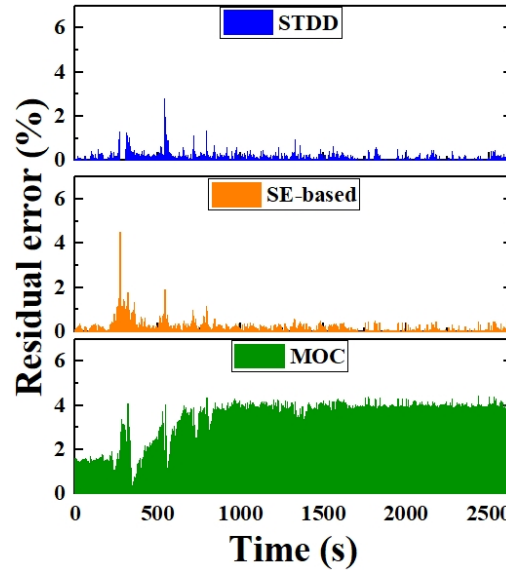


(ii) Outlet flowrate estimation

(c) Case 3



(i) Inlet flowrate estimation



(ii) Outlet flowrate estimation

(d) Case4

Figure B.3: Visualization comparison of absolute residual errors between SE-based method and STDD

Table B.3: MAPE comparisons of flowrate estimation between SE-based method and STDD

Cases	Methods	Inlet flowrate estimation (%)			Outlet flowrate estimation (%)		
		Whole flow process	Transient condition	Pseudo-steady condition	Whole flow process	Transient condition	Pseudo-steady condition
Case 2	STDD	<b>0.073</b>	<b>0.149</b>	<b>0.056</b>	<b>0.069</b>	<b>0.134</b>	<b>0.054</b>
	MOC	0.452	1.358	0.247	1.441	2.062	1.531
	SE-based	0.104	0.283	0.064	0.125	0.319	0.081
Case 3	STDD	<b>0.201</b>	<b>0.720</b>	<b>0.129</b>	<b>0.174</b>	<b>0.334</b>	<b>0.152</b>
	MOC	2.210	3.932	1.997	0.930	1.905	0.753
	SE-based	0.357	1.375	0.222	0.268	0.797	0.198
Case 4	STDD	<b>0.110</b>	<b>0.321</b>	<b>0.091</b>	<b>0.094</b>	<b>0.188</b>	<b>0.076</b>
	MOC	3.366	3.559	1.805	2.281	2.505	2.237
	SE-based	0.158	0.714	0.115	0.292	0.913	0.172

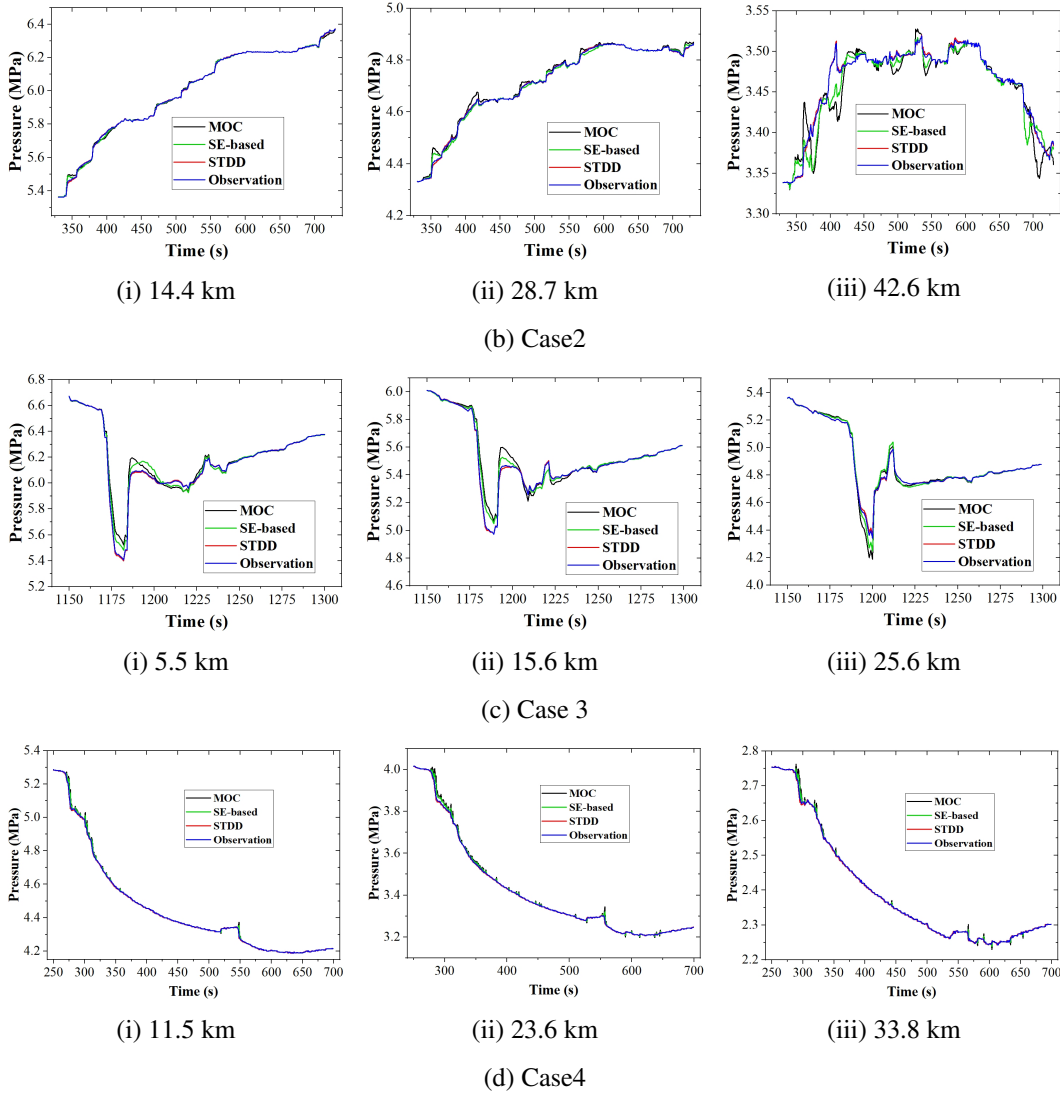


Figure B.4: Results comparison of simulated pressure at different locations between SE-based methods and STDD

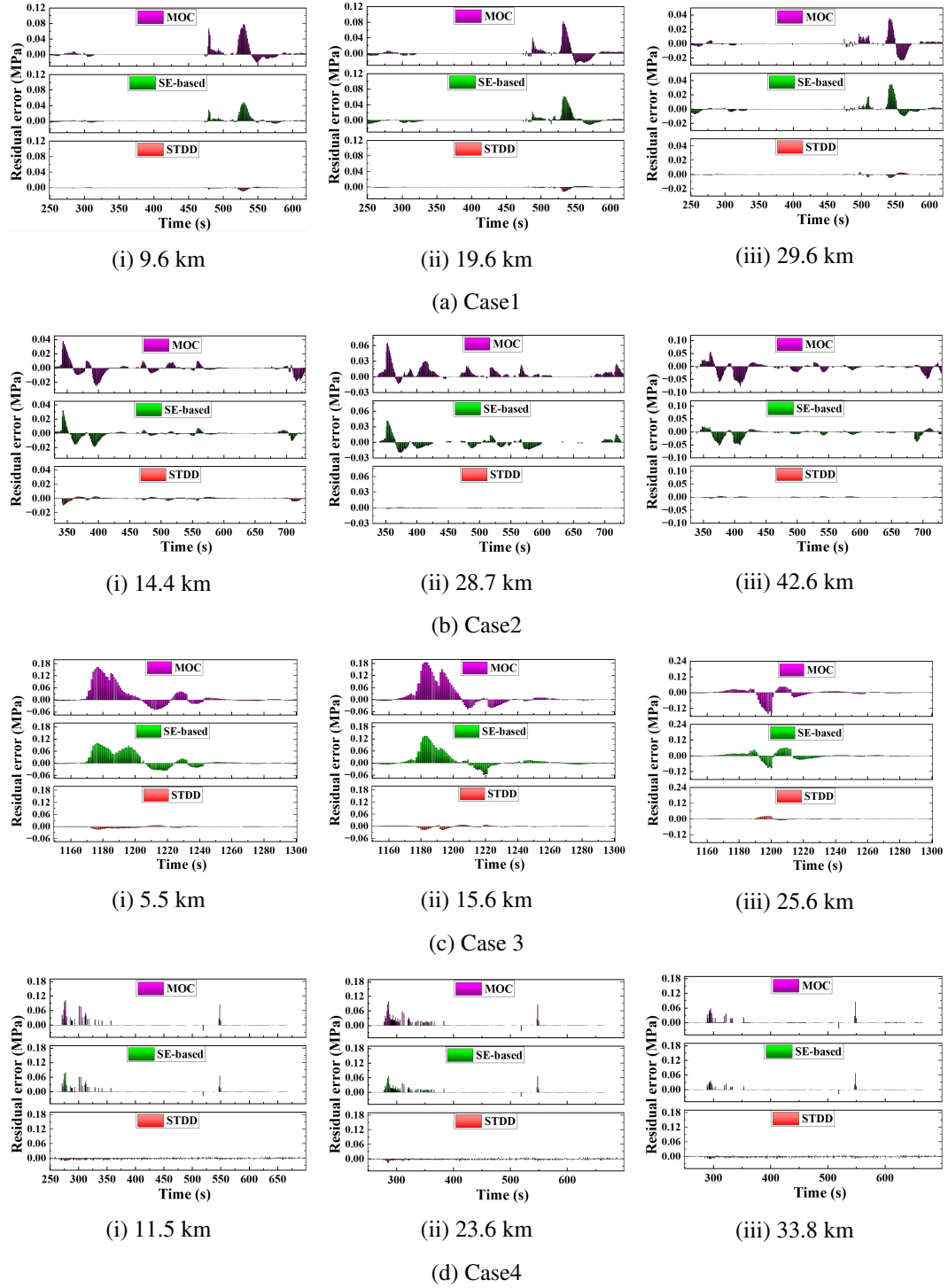
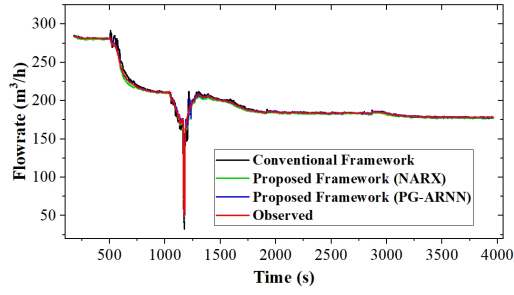
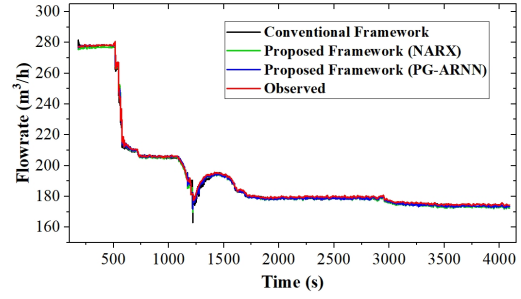


Figure B.5: Residuals comparison of simulated pressure at different locations between SE-based method and STDD

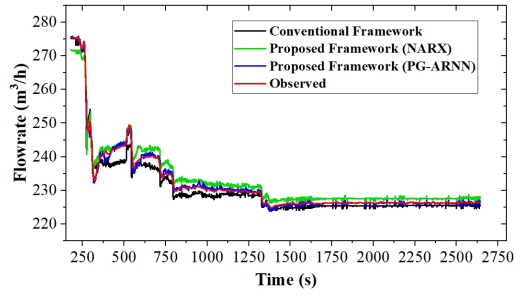


(i) Inlet flowrate estimation

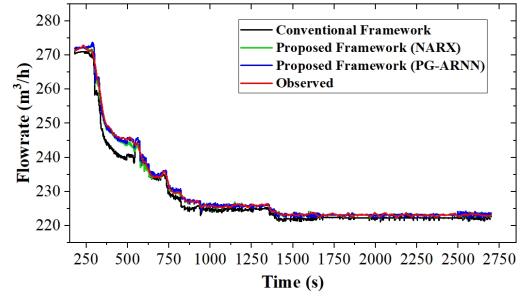


(ii) Outlet flowrate estimation

(c) Case 3



(i) Inlet flowrate estimation



(ii) Outlet flowrate estimation

(d) Case 4

Figure B.6: Results comparison of different online real-time simulation frameworks



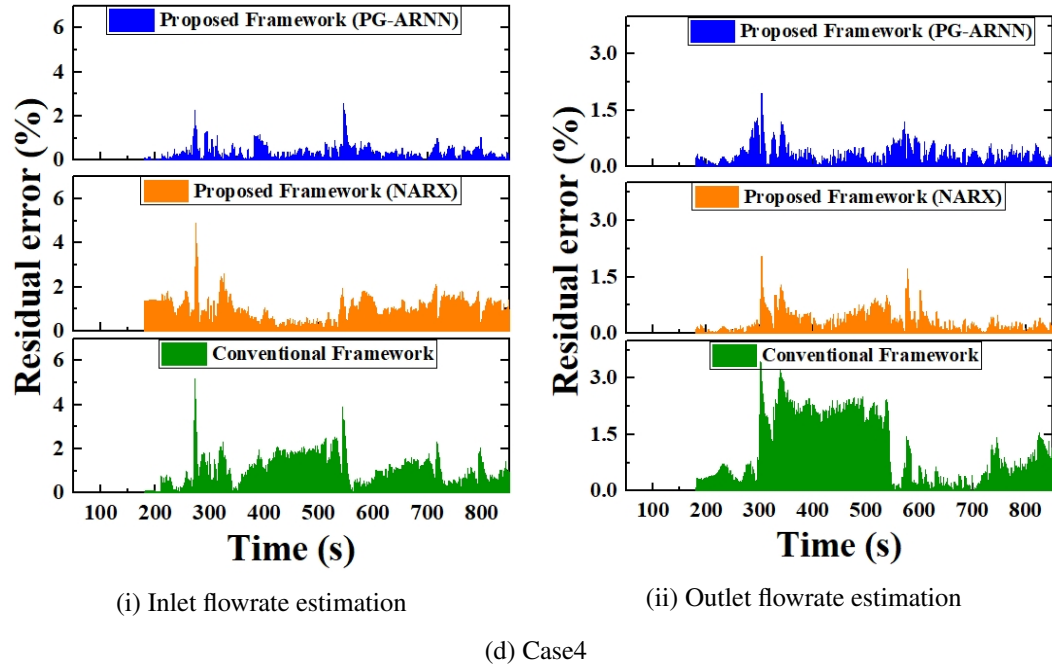
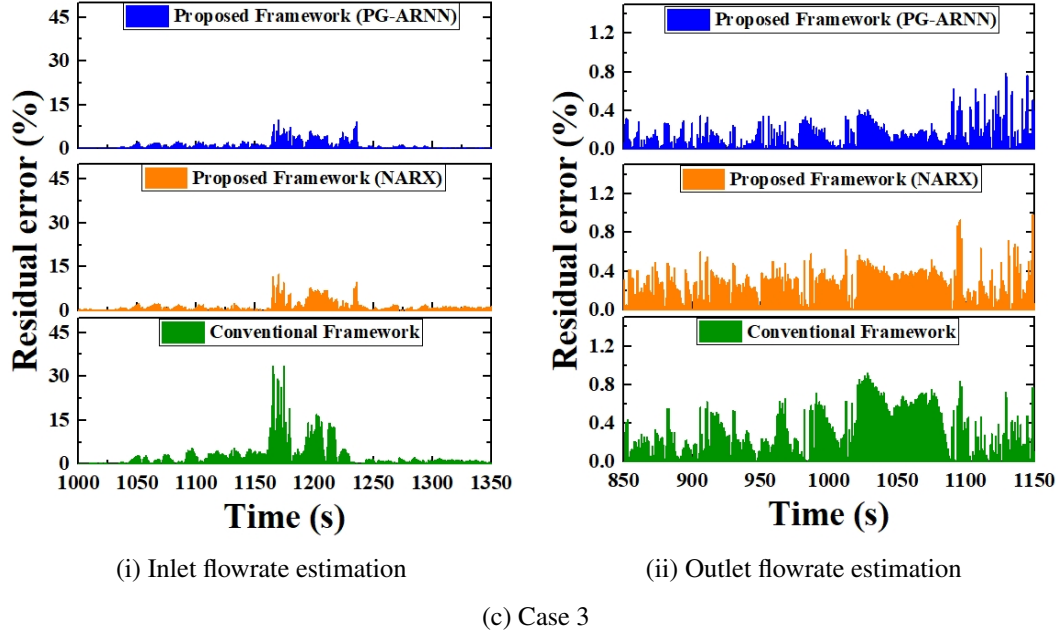


Figure B.7: Absolute residual errors of different online real-time simulation frameworks

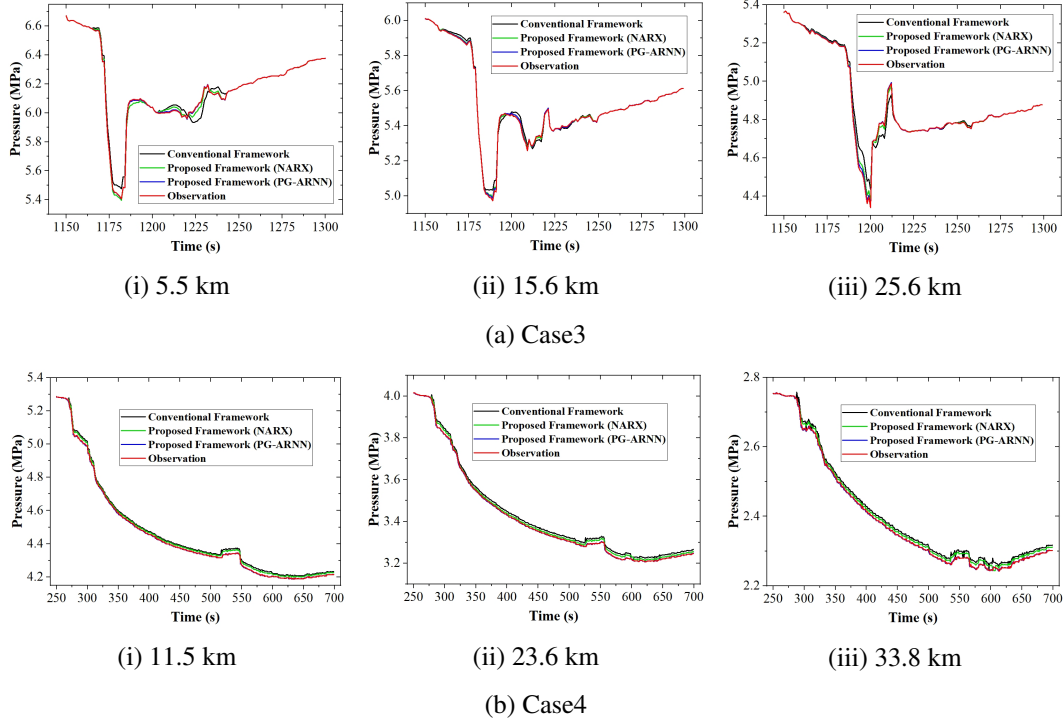


Figure B.8: Results comparison of simulated pressure at different locations between various frameworks

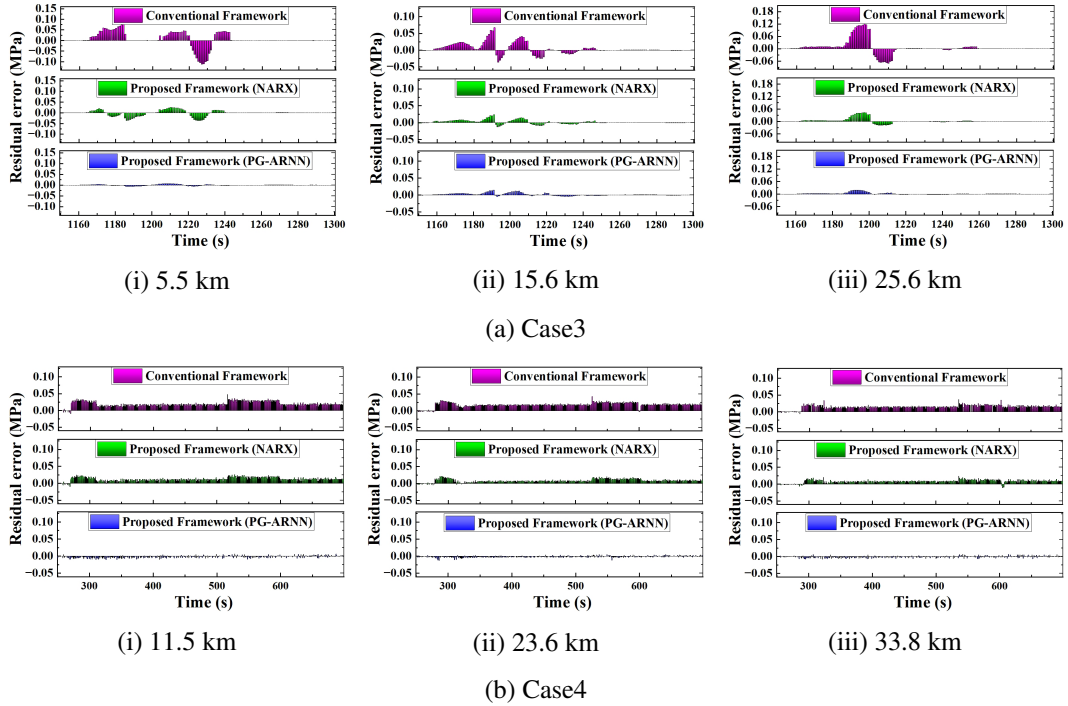


Figure B.9: Residual errors of simulated pressure at different locations between various frameworks

## C Additional Experimental Results

### C.1 Interpretability analysis of hydraulic spatiotemporal dynamics identification

As illustrated in Figure C.1, STDD is conducted at 10-second interval to identify friction coefficients across various cases. The results reveal a strong correlation between the friction coefficient and hydraulic parameters, with clear phase synchronization to flowrate dynamics. Notably, under pronounced flowrate fluctuations, the friction coefficient exhibits rapid transient changes. This highlights the physical interpretability of the proposed STDD, which captures variations in transient hydraulic behavior induced by friction changes through spatiotemporal derivative residuals. Furthermore, the larger objective values can be found during fast-transient process, which demonstrates the significant challenge in precisely reconstructing abrupt hydraulic dynamic features.

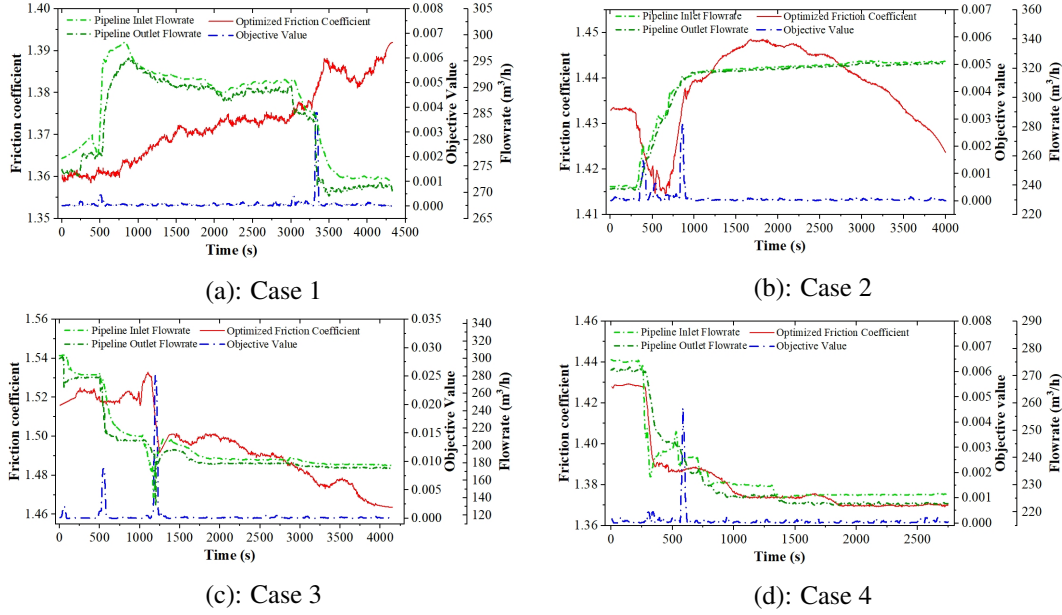


Figure C.1: Optimization results of friction coefficient with time interval being 10 seconds

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